Numerical simulations of high reactivity gasoline fuel sprays under vaporizing and reactive conditions

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Abstract

Gasoline compression ignition (GCI) engines are becoming more popular alternative for conventional spark engines to harvest the advantage of high volatility. Recent experimental study demonstrated that high reactivity gasoline fuel can be operated in a conventional mixing controlled combustion mode producing lower soot emissions than that of diesel fuel under similar efficiency and NOx level [1]. Therefore, there is much interest in using gasoline-like fuels in compression ignition engines. To improve the fidelity of simulation-based GCI combustion system development, it is mandatory to enhance the prediction of spray combustion of gasoline-like fuels. The purpose of this study is to model the spray characteristics of high reactivity gasoline fuels and validate the models with experimental results obtained through an optically accessible constant volume vessel under vaporizing [2] and reactive conditions [3]. For reacting cases, a comparison of PRF and KAUST multi-component surrogate (KMCS) mechanism was done to obtain good agreement with the experimental ignition delay. From this study, some recommendations were proposed for GCI combustion modelling framework using gasoline like fuels.

Introduction

Spray combustion depends highly on effective liquid fuel atomization, which controls the fuel evaporation rate and air-fuel mixing, and in turn dictates the emission levels and brake power of the engine [4]. Poor fuel atomization leads to non-uniform fuel-air mixing. Local inhomogeneity in the mixture composition can result in varied ignition and emission characteristics [5]. The fuel injection and spray break-up process are complex in nature, which involves turbulent and time-dependent two-phase flow. Consequently, modelling the spray phenomena is a challenging task, especially with the advent of new complex fuels.

Gasoline compression ignition (GCI) engines are becoming popular to exploit the advantage of higher fuel volatility and potentially lower aromatic content [1]. The development of GCI to low-temperature partially premixed compression ignition (PPCI) strategy can help in obtaining a better NOx-soot trade-off. Therefore, there is much interest in using gasoline-like fuels in compression ignition engines. Naphtha being a high reactivity gasoline fuel is one of the candidate fuels for advanced combustion engines [6,7].

Experimental conditions and fuel specification

The spray experiments were performed in an optically accessible constant volume chamber at Michigan Technological University (MTU). The chamber is a pre-burn type which combusts a gaseous mixture of acetylene and hydrogen to generate appropriate ambient conditions prior to the injection of fuel. The fuel injection event takes place during the combustion chamber cool down phase when exact ambient condition was reached. Further details of the experimental facilities can be found in Zhang et al. [2] and Meng et al. [3]. The nozzle used was a convergent single hole nozzle. The specifications of the injector are shown in table 1. The experimental initial and boundary conditions are listed in table 2.

Table 1. Fuel injector specifications

<table>
<thead>
<tr>
<th>Description</th>
<th>Single hole solenoid driven hydraulically lifted needle</th>
</tr>
</thead>
<tbody>
<tr>
<td>Outlet diameter (D_out) [μm]</td>
<td>176</td>
</tr>
<tr>
<td>K-factor</td>
<td>1.8</td>
</tr>
<tr>
<td>Cs (Re=12000)</td>
<td>0.94</td>
</tr>
</tbody>
</table>

Table 2. Experimental initial and boundary conditions

<table>
<thead>
<tr>
<th>Injection pressure [MPa]</th>
<th>100-150-200</th>
</tr>
</thead>
<tbody>
<tr>
<td>Injection duration [ms]</td>
<td>~&gt;3.0</td>
</tr>
<tr>
<td>Ambient temperature [K]</td>
<td>800-1200</td>
</tr>
<tr>
<td>Ambient pressure [MPa]</td>
<td>3-6-10</td>
</tr>
<tr>
<td>Ambient Oxygen [%]</td>
<td>0, 15</td>
</tr>
</tbody>
</table>
The fuel used is high reactivity gasoline. The Research Octane Number (RON) of the fuel is 58.8 which is lower than typical gasoline (RON 91). It has an equivalent Cetane Number (CN) of 33.7. This high reactivity gasoline has lower cetane number and contains less aromatics and high volatility in nature compared to that of diesel fuel. The properties of the fuel used in this study is shown in table 3 in comparison to that commercial diesel and gasoline (RON 91).

Table 3. Fuel properties

<table>
<thead>
<tr>
<th>Fuel</th>
<th>High reactivity gasoline</th>
<th>Diesel</th>
<th>Commercial gasoline</th>
</tr>
</thead>
<tbody>
<tr>
<td>RON</td>
<td>58.8</td>
<td>-</td>
<td>91.4</td>
</tr>
<tr>
<td>MON</td>
<td>57.9</td>
<td>-</td>
<td>84.6</td>
</tr>
<tr>
<td>AKI</td>
<td>58.4</td>
<td>-</td>
<td>88.0</td>
</tr>
<tr>
<td>CN</td>
<td>33.7</td>
<td>43.7</td>
<td>20.4</td>
</tr>
<tr>
<td>Density [kg/m³]</td>
<td>705</td>
<td>841</td>
<td>733</td>
</tr>
<tr>
<td>Kinematic viscosity [mm²/s]</td>
<td>0.58</td>
<td>2.25</td>
<td>0.55</td>
</tr>
<tr>
<td>H/C ratio</td>
<td>2.124</td>
<td>1.834</td>
<td>1.854</td>
</tr>
<tr>
<td>Aromatics [% vol.]</td>
<td>9.1</td>
<td>29.7</td>
<td>25.7</td>
</tr>
<tr>
<td>Olefins [%vol.]</td>
<td>0.4</td>
<td>29.7</td>
<td>10.4</td>
</tr>
<tr>
<td>Sulfur [ppm]</td>
<td>19.3</td>
<td>11.9</td>
<td>3.0</td>
</tr>
<tr>
<td>IBP [°C]</td>
<td>32.3</td>
<td>176</td>
<td>34</td>
</tr>
<tr>
<td>10% [°C]</td>
<td>58.2</td>
<td>206</td>
<td>51</td>
</tr>
<tr>
<td>50% [°C]</td>
<td>94.4</td>
<td>249</td>
<td>83</td>
</tr>
<tr>
<td>90% [°C]</td>
<td>124.0</td>
<td>303</td>
<td>151</td>
</tr>
<tr>
<td>FBP [°C]</td>
<td>139.7</td>
<td>337</td>
<td>198</td>
</tr>
<tr>
<td>Net Heat Value [MJ/kg]</td>
<td>43.363</td>
<td>42.818</td>
<td>43.42</td>
</tr>
</tbody>
</table>

Numerical methodology

Fuel spray and combustion simulations were performed using a Eulerian-Lagrangian approach in the commercial CFD code CONVERGE. It incorporates various models for spray injection, atomization, break-up, turbulence, droplet collision, coalescence and evaporation. For turbulence modeling, the RANS-based renormalization group (RNG) k-ε model was used. These equations are solved by using a finite volume solver. The spray break-up was modeled using the modified Kelvin-Helmholtz Rayleigh-Taylor (KH-RT) model without an ad hoc break-up length.

The computational domain is a cylinder of 100 mm in diameter and 100 mm in height. CONVERGE generates the computational grid during runtime. The base grid size is fixed at 2 mm. To resolve the near-nozzle spray development process in detail, a fixed embedding is employed such that the minimum grid size is 0.25 mm. In addition to fixed embedding, three levels of adaptive mesh refinement (AMR) were employed for the velocity field. Figure 1 shows the mesh generated by CONVERGE with fixed embedding and AMR over the base grid at 0.5 ms after the start of injection (ASOI).

In the simulations, the fuel liquid properties were generated from Aspen HYSYS [8]. This has been extensively validated in previous studies [1,9]. The fuel liquid properties of high reactivity gasoline used in this simulation are shown in fig. 2 in comparison with that of the properties of diesel and gasoline fuels from CONVERGE database.

Two different mechanism were used in this study 1) PRF mechanism by An et al. [11,12] and 2) reduced KAUST Multi-Component Surrogate (KMCS) mechanism. The PRF mechanism consists of 80 species and 204 reactions. The new KMCS mechanism was reduced from detailed mechanism by Sarathy et al. [13] using CHEMKIN-Pro with tolerance of 2%. The new reduced KMCS mechanism consists of 111 species and 456 reactions. The composition of high reactivity gasoline multi-component surrogate is given in table 4.

Figure 1. Grid generated by CONVERGE at 0.5 ms ASOI.
Table 4. Composition of high reactivity gasoline multi-component surrogate

<table>
<thead>
<tr>
<th>Species</th>
<th>Chemical formula</th>
<th>Mole fraction</th>
</tr>
</thead>
<tbody>
<tr>
<td>N-Pentane</td>
<td>C₅H₁₂</td>
<td>0.14</td>
</tr>
<tr>
<td>N-Heptane</td>
<td>C₇H₁₈</td>
<td>0.24</td>
</tr>
<tr>
<td>2-Methylheptane</td>
<td>C₇H₁₆</td>
<td>0.20</td>
</tr>
<tr>
<td>Toluene</td>
<td>C₇H₈</td>
<td>0.11</td>
</tr>
<tr>
<td>Cyclopentane</td>
<td>C₅H₁₀</td>
<td>0.09</td>
</tr>
</tbody>
</table>

Results and discussion

Liquid penetration and vapor penetration are used for validation. Liquid penetration is defined as the axial location encompassing 95% of the injected mass at that instant of time. Vapor penetration is defined as the farthest downstream location of 0.01% fuel mass fraction contour at that instant. For validation purposes, the liquid and vapor penetration measurements of high reactivity gasoline fuel at injection pressure of 150MPa, ambient pressure of 3MPa and ambient temperature of 1000 K were employed.

Effect of spray angle

To study the effect of spray angle on the liquid and vapor penetrations, average experimental spray angle and experimental spray angle over time were given as input. The experimental spray angle was given as input using a lookup table. Figure 3 shows the experimental spray angle over time and time-averaged value calculated from the experiment. Figure 4 shows the effect of different spray angle inputs on liquid and vapor penetration of high reactivity gasoline fuel. The transient spray angle input over time using a lookup table gives better predictions than just using a single time-averaged spray angle. It should also be noted that initial over prediction of liquid length is overcome by using transient spray angle. Therefore, using more detailed experimental values for spray angle improves fidelity of the simulation results.

Effect of KH-RT model constant

Three values of the KH time constant $B_1$ were chosen. They are the default value of 7, larger value of 10 and smaller value of 5. Similarly, three values of RT break-up model size constant, $C_{RT}$, were chosen. They are the default value of 0.1, and two larger values of 0.5 and 1.0. Vapor and liquid penetration of high reactivity gasoline fuel with these different constants are shown in Figure 5 and 6. Fig. 5 shows that the liquid penetration is affected by the KH time constant $B_1$, but vapor penetration shows a negligible change. Both liquid and vapor penetration show a negligible change with RT model size constant as shown in fig. 6. From the simulation results, the baseline values for $B_1$ and $C_{RT}$ are considered as the default values of 7 and 0.1, respectively.

Figure 2. Liquid properties of high reactivity gasoline generated from Aspen HYSYS, diesel and gasoline properties from CONVERGE.

Figure 3. Transient experimental spray angle for high reactivity gasoline fuel.
Effect of droplet collision models

Two different droplet collision models, O’Rourke [14] and no time counter (NTC) [15], were studied. Once a collision occurs, the outcomes are predicted as bouncing, stretching, reflexive separation, or coalescence [16]. Figure 7 shows the effect of different collision models on liquid and vapor penetrations of high reactivity gasoline fuel. Both methods show a negligible effect on the liquid and vapor penetrations. However, the NTC method involves stochastic sub-sampling of the parcels within each drop. This results in much faster collision calculations compared to O’Rourke method. In O’Rourke’s method, the computational cost increases with the square of the number of parcels whereas, in the NTC method, the cost is linear. Furthermore, O’Rourke’s method assumes that multiple collisions can occur between parcels and this process is governed by Poisson distribution. The Poisson distribution is incorrect unless collision has no consequences for the parcels. Since the collision changes the velocities, size and number of parcels, the method of repeated sampling used by the NTC method generates more accurate results. Therefore, the NTC collision model was considered to be the baseline model for further studies.

Effect of droplet evaporation models

Two different droplet evaporation models, Frossling [17] and Chiang [18], have been tested. Figure 8 shows the effect of different droplet evaporation models on liquid and vapor penetrations of high reactivity gasoline fuel. The Chiang droplet evaporation model predicts longer liquid length compared to the Frossling evaporation model. However, a negligible change was observed in the vapor penetration length. The Chiang model includes the effect of convection, accounting for the effects of variable thermo-physical properties, transient heating and internal circulation of liquid, deceleration of the flow due to the drag of the droplet, boundary layer blowing and moving interface by introducing correction factors in the calculation of Sherwood and Nusselt numbers. Therefore, when using this model, the heat diffusion from gas phase to the droplet is lower than that of the Frossling model. Hence, Chiang model predicts a longer liquid length. Despite the detailed Chiang model, Frossling model captures enough evaporation physics to predict the spray characteristics on par with experiments. Therefore, the Frossling model was chosen to be the baseline evaporation model for further studies.
Figure 6. Effect of different RT model constant $C_{RT}$ on liquid and vapor penetration of high reactivity gasoline fuel.

**Spray Morphology**

The temporal evolution of fuel vapor mass fraction of high reactivity gasoline is shown in Fig. 9 for the baseline case. The experimental images shown is for single test realization. The simulation used transient spray angle, KH time constant, $B_1$ as 7, RT break-up model size constant, $C_{RT}$ as 0.1, NTC collision model and Frossling droplet evaporation model. It can be observed that the simulation results qualitatively agree with the experimental data quite well at different timings.

**Effect of ambient temperature**

The effect of ambient temperature is studied by varying it at ambient pressures of 3MPa and 6MPa and fuel injection pressure of 150MPa. Fig. 10 shows the liquid length comparison between experiment and simulation under ambient pressure of 3 and 6MPa at varying ambient temperature between 800-1200K. Only two temperature variants are studied in experiment under ambient pressure of 3MPa due to experimental constraint in achieving appropriate boundary conditions at such low ambient pressure. It can be seen that simulations capture the liquid length very well on par with the experiments. At ambient pressure of 6MPa, the liquid length is almost insensitive to changes in the ambient temperature. It is interesting to note that the model is able to capture this trend and behavior very well. Fig. 11 shows the comparison of vapor penetration under varying temperature and ambient pressure of 3MPa. At higher ambient temperatures, the vapor penetration length is longer due to lower ambient densities. It can be found that the model shows good prediction the vapor penetration lengths.

Figure 7. Effect of different collision models on liquid and vapor penetration of high reactivity gasoline fuel.

Figure 9. Temporal evolution of simulated fuel vapor mass fraction compared to experimental images.
Figure 8. Effect of different evaporation models on liquid and vapor penetration of high reactivity gasoline fuel.

Figure 10. Comparison of experimental and simulation liquid length of high reactivity gasoline fuel under varying temperature at ambient pressure of 3MPa.

Simulation of reacting sprays

Fig. 12 shows the comparison of predicted ignition delay of high reactivity gasoline fuel by two mechanisms with that of experiment in constant volume combustion chamber from MTU [3]. A wide range of temperatures (800-1200K) under ambient pressure of 6MPa, injection pressure of 150MPa and 15% ambient oxygen were used for validation of the mechanisms. It is found that the PRF mechanism consistently under-predicts the ignition delay, whereas the new multi-component surrogate (KMCS) mechanism predicts the ignition delay in good agreement with experiments. This shows that the new KMCS mechanism along with the thermo-physical properties used in the simulations performs well under heavy duty engine conditions.

In addition to the constant volume ignition delay validation, comparisons were made for the predicted heat release rate (HRR) by two mechanisms with that of experimental data. Fig. 13 shows the heat release rates of the simulations and experiment at ambient pressure of 6MPa, injection pressure of 150MPa and 15% oxygen. The heat release rates are calculated using the following equation for both experiment and simulation

\[
\frac{dQ}{dt} = \frac{1}{\gamma - 1} V \frac{dP}{dt}
\]

where, \( \frac{dQ}{dt} \) is HRR, P is the pressure, V is the volume and \( \gamma \) is the specific heat ratio.
and vapor penetrations of vaporizing sprays were investigated. From the simulation results, the baseline values of model constants and baseline sub-models were determined for vaporizing spray conditions. The following recommendations are derived for simulating high reactivity gasoline fuel

1. For the KH-RT model, the two major constants, $B_1$ and $C_{RT}$, are set as 7 and 0.1, respectively.
2. The NTC collision model is preferred over O’Rourke model for computational cost consideration.
3. The Frossling droplet evaporation model yields better prediction than the Chiang model for droplet evaporation.
4. The new KMCS mechanism predicts both the ignition delay and heat release rate in good agreement with the experimental data compared to that of PRF mechanism.

References


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